

## NOTES

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## Synthetic Inorganic Ion-exchange Materials. XIII. The Mutual Separation of Alkali Metals with Three Different Antimonic Acids

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The present paper will describe the use in the chromatographic separation of alkali metal ions on columns of the three different antimonic acids;<sup>1)</sup> amorphous ( $S_A$ ), glassy ( $S_G$ ), and crystalline ( $S_C$ ). The samples were prepared as was been described in a preceding paper,<sup>2)</sup> and then controlled

TABLE 1. DISTRIBUTION COEFFICIENTS AND SEPARATION FACTORS ( $\alpha$ ) ON THREE DIFFERENT ANTIMONIC ACIDS

Exchanger	Solution	Li	Na	K	Rb	Cs
$S_A$	$1 \times 10^{-3}M$ $MNO_3$	$1.0 \times 10^2$	$4.1 \times 10^2$	$1.5 \times 10^3$	$2.8 \times 10^3$	$5.8 \times 10^3$
	$0.1N$ $HNO_3$	6.4	27.8	123	196	226
	( $\alpha$ )	4.3	4.4	1.6	1.2	
$S_G$	$0.05M$ $NH_4NO_3$	7.7	24.8	41	41	31
	( $\alpha$ )	3.2	1.7	1.0	0.76	
	$1 \times 10^{-3}M$ $NMO_3$	$2.6 \times 10^2$	$7.5 \times 10^2$	$2.5 \times 10^3$	$6.0 \times 10^3$	$9.8 \times 10^3$
$S_C$	$0.1N$ $HNO_3$	10.4	37.4	167	238	318
	( $\alpha$ )	3.6	4.4	1.4	1.3	
	$0.05M$ $NH_4NO_3$	12.5	37.5	55	44	37.3
	( $\alpha$ )	2.5	1.7	0.8	0.85	
		Li	K	Cs	Rb	Na
$S_C$	$1 \times 10^{-3}M$ $MNO_3$	$7.1 \times 10$	$1.76 \times 10^4$	$3.5 \times 10^4$	$1.3 \times 10^5$	$1.0 \times 10^6$
	$0.1N$ $HNO_3$	0.9	$4.5 \times 10^2$	$1.4 \times 10^3$	$8.1 \times 10^3$	$8.3 \times 10^4$
	( $\alpha$ )	500	3.1	5.8	10.2	
	$0.05M$ $NH_4NO_3$	2.5	10.4	37.3	56.2	890
	( $\alpha$ )	4	3.6	1.5	15.8	
		Li	Na	K	Rb	Cs
Amberlite IR-120	$1 \times 10^{-3}M$ $MNO_3$	$1.6 \times 10^3$	$3.1 \times 10^3$	$4.2 \times 10^3$	$7.8 \times 10^3$	$1.3 \times 10^4$
	$0.2N$ $HNO_3$	19.5	30	64	85.5	100
	( $\alpha$ )	1.5	2.1	1.3	1.2	
Zirconium phosphate	$1 \times 10^{-3}M$ $MNO_3$	$1.7 \times 10^3$	$1.1 \times 10^3$	$3.8 \times 10^3$	$9.8 \times 10^3$	$1.9 \times 10^4$
	$0.1N$ $HNO_3$	15.0	41	140	390	910
	( $\alpha$ )	2.7	3.4	2.8	2.3	

Exchanger: 0.100 g, total volume: 25.0 ml,  $20 \pm 0.05^\circ C$ , immersion; 24 hr. $S_A$ : amorphous antimonic acid,  $S_G$ : glassy antimonic acid,  $S_C$ : crystalline antimonic acid.

Distribution coefficient was calculated from the following equation;

$$K_d = \frac{A_0 - A_s}{A_s} \cdot \frac{ml}{g}$$

where  $A_0$  is the concentration of alkali metal in the solution before equilibration ( $1 \times 10^{-3}$  mol/l),  $A_s$  is the concentration in the solution after equilibration, ml is total volume of the solution in milliliters, and g is the weight of the sample in grams.

1) M. Abe and T. Ito, This Bulletin, **41**, 333 (1968).2) M. Abe and T. Ito, *ibid.*, **41**, 2366 (1968).

in a 100–200 mesh size. The column experiments were carried out with a column ( $0.8\phi \times 6.0$  cm) containing 3.0, 6.4, and 3.9 g for  $S_A$ ,  $S_G$ , and  $S_C$  respectively. The concentration of alkali metals was determined flame-photometrically by using a Hitachi EPU-2A with a flame apparatus, H-2, attached.

### Results and Discussion

**Affinity Series for Alkali Metal Ions.** Table I gives the values of the distribution coefficients for alkali metal ions on three different antimonite acids. The  $K_d$  values on  $S_C$  are higher than those on  $S_A$  and  $S_G$  except in the case on  $Li^+$  adsorption, and  $S_A$  gives values almost identical with those obtained on  $S_G$ . The affinity on the  $S_A$  and  $S_G$  was found to increase in the order:  $Li^+ < Na^+ < K^+ < Rb^+ < Cs^+$  in the acid solution, while the order was:  $Li^+ < Na^+ \approx Cs^+ < K^+ = Rb^+$  in the ammonium nitrate solution. The affinity series on the  $S_C$  may be written as  $Li^+ < K^+ < Cs^+ < Rb^+ < Na^+$  in the acid solution and  $Li^+ < K^+ < Rb^+ < Cs^+ < Na^+$  in the ammonium nitrate solution. The difference in selectivity is very large compared with those obtained for the sulfonic acid resins. In the acid solution,  $Rb^+$  was more strongly adsorbed than  $Cs^+$ , with the separation factor of 5.8.  $Na^+$  was more strongly adsorbed than any other alkali metal ions in the solutions of both nitric acid and ammonium nitrate. The separation factor in the pairs of lithium and other alkali metals may be compared favorably with those of other cation exchangers.

According to Lefebvre,<sup>3)</sup> the inverse selectivity should prevail for alkali metals:  $Na^+ < K^+ < NH_4^+ < Rb^+ < Cs^+$  on the polyantimonite acid.

When a large volume of a 0.1N solution of various alkali metal salts was passed through an  $S_C$  column, the uptake of alkali metals showed the values of 1.0, 2.8, 2.4, 1.4, and 1.2 meq/g for  $Li^+$ ,  $Na^+$ ,  $K^+$ ,  $Rb^+$ , and  $Cs^+$  respectively. In the solutions with a constant ionic strength of 0.1M ( $HNO_3 + MnO_3$ ), ion-exchange isotherms on the  $S_C$  gave ogce-sharp curves,<sup>4)</sup> as is the case with rigid inorganic ion-exchangers (*e. g.*, zirconium phosphate, zeolites, and basic cancrinite). These results indicate that the selectivity coefficient varies strongly with the ionic composition and that the reversal of selectivity, which may be due to steric factors, arises from the course of conversion. The crystalline antimonite acid presents a fairly rigid lattice, for the volume change on conversion from the hydrogen form to the alkali forms is very small; accordingly, the

lattice constants of various forms gave 10.30, 10.33, 10.37, 10.38, 10.40 and 10.47 Å for Na, Rb, Li, H, Cs, and K forms, without any change in the crystal system. The increased order in the lattice constant conforms to the inverse order in the affinity series for micro amounts of all the alkali metal ions except  $Li^+$ .

**Separation of Alkali Metal Ions on the Columns of the Three Different Antimonite Acids.** Small amounts of various alkali metal ions were adsorbed onto the column and then eluted with different eluants.

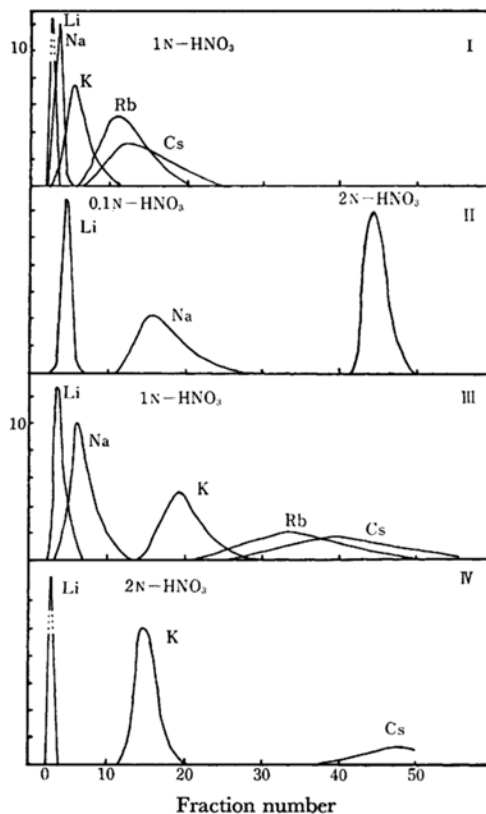


Fig. 1. The elutions of alkali metals with nitric acid of various concentrations on the three different antimonite acids.

Fraction: 5.5 ml, alkali metal: each 0.02 mmol, flow rate; 0.3 ml/min

I and II: amorphous antimonite acid, III: glassy antimonite acid, IV: crystalline antimonite acid.

### Elution with Various Nitric Acid Solutions.

On the  $S_A$  and  $S_G$ , all of the alkali metal ions were more easily eluted with nitric acid of a relatively dilute solution than in the case of  $S_C$ , and the elution curves were always somewhat asymmetric. Complete separation were made for  $Li^+$ ,  $Na^+$ , and  $K^+$  with an 0.1N ( $S_A$ ) or 0.2N ( $S_G$ ) and 2N nitric acid solution. On  $S_C$ , a good separation was obtained for  $Li^+$ ,  $K^+$ , and  $Cs^+$  with a 2N nitric acid solution, but  $Na^+$  and  $Rb^+$  were not eluted within 70 fractions.

3) J. Lefebvre and F. Gamard, *C. R. hebdomadaire. Seances Acad. Sci., Paris*, **260**, 6911 (1965).

4) M. Abe and T. Ito, Preprints for The 19th Annual Meeting of The Chemical Society of Japan (April, 1966) Vol. II, p. 292.

It has been established that, on the organic ion-exchangers, the mutual separation between  $\text{Rb}^+$  and  $\text{Cs}^+$  is very difficult. The separation on the  $S_C$  can be made completely with a 4N nitric acid solution. The separation factor,  $\alpha_{\text{Rb}}^{\text{Cs}}$ , calculated from the peak volume in the elution curves showed 5.6. Sodium ions were more strongly adsorbed than any other alkali metal ions and could not be eluted by a relatively concentrated nitric acid solution within the column volume shown in Fig. 2-I. Figure 2-II shows that the order of peak

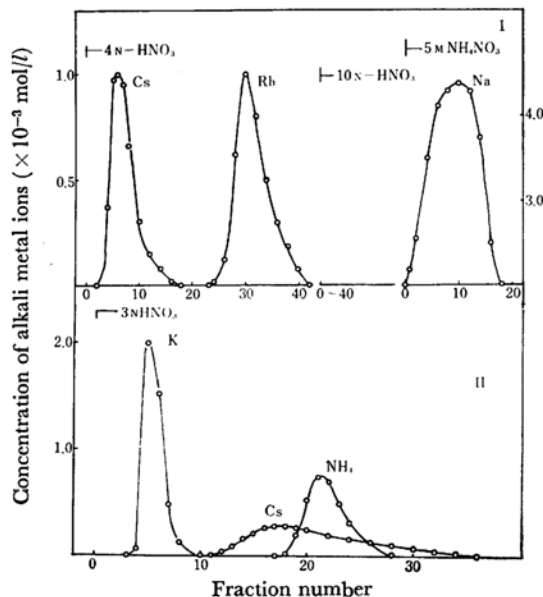


Fig. 2. The elution of alkali metals on crystalline antimonite acid

I: separation of sodium, rubidium and cesium fraction; 5.5 ml, Rb and Cs; each 0.04 mmol, Na; 0.1 mmol

II: elution of potassium, cesium and ammonium, ions

fraction; 5.6 ml, K, Cs and  $\text{NH}_4$ ; each 0.02 mmol

Flow rate: 0.3 ml/min.

volume in the elution curves was  $\text{K}^+ < \text{Cs}^+ < \text{NH}_4^+$  and that  $S_C$  was not selective for ammonium and cesium ions, while there was a broader curve for cesium ions. With eluants of both nitric acid and ammonium nitrate solutions, the time required was relatively short, only about 10 hr being sufficient for a complete separation of a milligram-amount of alkali metals (Fig. 3-I).

**Elutions with Various Ammonium Nitrate Solutions.** On  $S_C$ , pairs of neighbouring alkali metal ions, such as Li-K, K-Rb, and Cs-Na, were

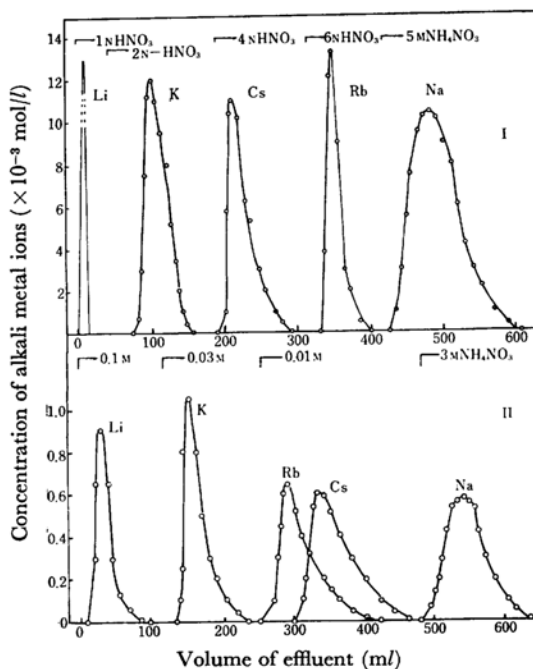


Fig. 3. The separation of alkali metal ions with nitric acid and ammonium nitrate of various concentration on the crystalline antimonite acid  $S_C$ . Flow rate: 0.6 ml/min.

I: with the nitric acid and ammonium nitrate solutions, Li; 0.01 mmol, Na; 0.1 mmol, K, Rb, Cs; each 0.04 mmol

II: with the ammonium nitrate solutions, Li; 0.02 mmol, Na, K, Rb, Cs; each 0.04 mmol

easily separated in the same column length, but not the Rb-Cs pair (Fig. 3-II). On  $S_A$  and  $S_G$ , all the alkali metal ions except  $\text{Li}^+$  were removed as a group with a 0.03M ammonium nitrate solution.

These results indicate the presence of antimonite acid of two types, with a different selectivity for alkali metal-ions adsorptions, a difference may be closely related to the disparity in the surface structure.<sup>2)</sup> The  $S_G$  and  $S_C$  were favorable for column work because their lower solubilities and their suitable granular forms. The  $S_C$  was especially stable against almost all reagents, including concentrated acid and alkaline solutions and oxidizing agents. The  $S_A$  was unsuitable, since it was relatively soluble in water and was gradually transformed into crystalline antimonite acid in a relatively concentrated acid solution.

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